AMENDMENTS TO THE DETAILED DESCRIPTION

Please amend the specification as follows:

Please replace paragraph [00111] with the following replacement paragraph:

[00111] Propylene was polymerized as follows in a two reactor system. The polymerization was conducted in a pilot scale continuous stirred tank, bulk liquid phase polymerization process employing two reactors in series. The reactors were equipped with jackets for removing the heat of polymerization. The reactor temperature was set at about 50 to 75 °C, with 5 to 10 °C difference between the reactors. Catalyst was fed at a rate of about 2 to 4 gm/hr. A 1 wt% solution of triethylaluminum (TEAl) in hexane was employed as a scavenger and added at a level of 20 wppm based on the weight of propylene fed to the reactor. Propylene was fed at a rate of about 100 to 110 kg/hr. Resin was removed at a rate of 50 to 100 lbs / hr. After eight days of continuous polymerization, the reaction was stopped and the reactors opened for inspection. A thick buildup of foulant was found on the agitator and baffles in one of the reactors.

Please replace paragraph [00112] with the following replacement paragraph:

[00112] Propylene was polymerized as in Example 1. A solution of Stadis® 425 was diluted in high purity hexane to a concentration of 0.024 % by weight of the antistatic agent solution to the hexane diluent. This solution was mixed with the 1 % by weight solution of TEAl in hexane prior to being injected into the reactor. The residence time of mixing was between four and ten minutes and the ~~ratio~~ weight percentage of the antistatic agent solution (active ingredients + solvent) to catalyst solids was between 1.1 and 1.5 % by weight. After approximately eight days of continuous polymerization, the reaction was stopped, reactors opened, and found to be clean and free of foulant buildup. A reduction in catalyst activity (pounds of polymer produced / pounds of catalyst consumed) of approximately 10 % was observed compared to Example 1.